



# ZERO BRINE

## Work Package 2

Re-designing the supply chain of water and minerals in the multi-company site of the Energy Port and Petrochemical cluster in Botlek area



H2020 project, June 2018

# Objective

- Demonstrate NF – Evaporation concept for the treatment of IX regenerates and their subsequent exploitation for regeneration of IX-resins (internal valorization)
- Demonstrate AIX – NF – Evaporation – EFC concept
- Combine waste heat and wastewater streams in a multi-company site environment with the aim to eliminate brine effluent of the industrial water supplier, to recover high purity magnesium and to recycle streams within the site

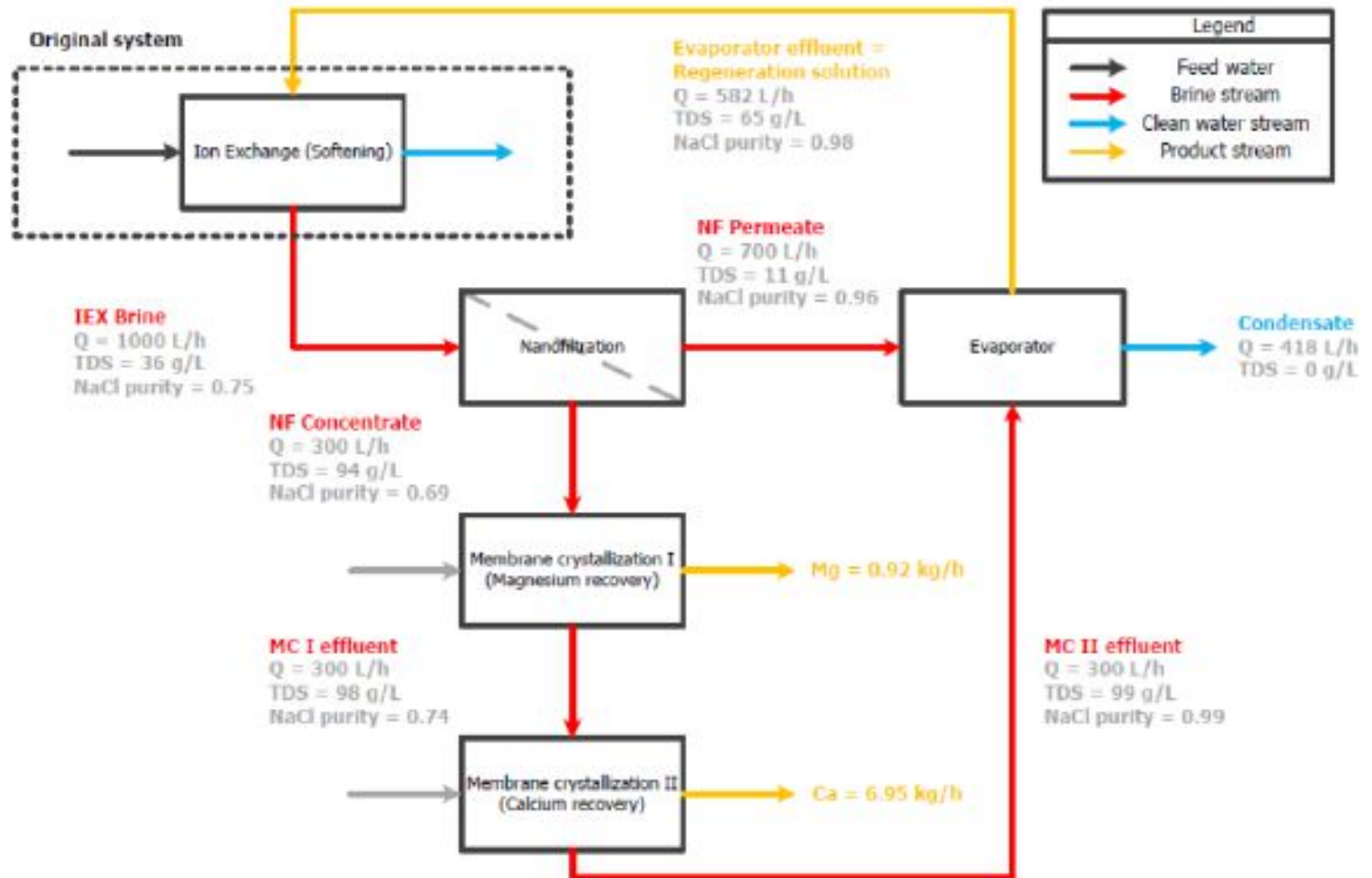
# Tasks

- 2.1: Preliminary design considerations (TU DELFT, NTUA, LENNTECH, EVIDES, UNIPA) [1-12]
  - 2.1.1: Determination of main brine treatment plant components for EVIDES SITE I [1, ~6]
  - 2.1.2: Determination of main components for EVIDES case II [7, ~6]
- 2.2: Design, manufacturing and installation of the demo plants (NTUA, LENNTECH, TU DELFT, UNIPA, ARVIA) [7-24, ~14]
  - 2.2.1: Final engineering design of the brine treatment systems for EVIDES Site I & II
  - 2.2.2: Manufacturing large demo and pilot system components (**TU DELFT**, LENNTECH, NTUA, UNIPA, ARVIA)
  - 2.2.3: Assembling and installation of the large demo and pilot plants at the site of EVIDES, in the Botlek area (**LENNTECH**, NTUA, UNIPA, EVIDES)
- 2.3: Operation, optimization and assessment of the large-scale demonstration plants (**EVIDES**, TU DELFT, NTUA, LENNTECH, ARVIA, UNIPA) [19-42]
- 2.4: Data collection from demo plants at EVIDES Site I and Site II – Input for WP1, WP7, WP8, WP9, WP10 (**TU DELFT**) [1-42]

# Deliverables

- D2.1 : Report on the results from the simulations using PHREEQC [6]
- D2.2 : Report on physicochemical analyses on the wastewater compositions [6]
- D2.3 : Report on the bench-scale tests using equipment from the BEC [10]
- D2.4 : Report explaining the design procedure [18]
- D2.5 : Detailed engineering drawings [18]
- D2.6 : Report on the operation and optimization process [42]
- D2.7 : Database of data collected during WP2 demonstration activity [6]

# Pilot 1 Botlek



# D2.1 PHREEQC

Composition of NF concentrates at 50% and 70% recovery

Elem. or ion	Sample 1				Sample 2			
	50% recovery		70% recovery		50% recovery		70% recovery	
	mg.L <sup>-1</sup>	mol.L <sup>-1</sup>	mg.L <sup>-1</sup>	mol.L <sup>-1</sup>	mg.L <sup>-1</sup>	mol.L <sup>-1</sup>	mg.L <sup>-1</sup>	mol.L <sup>-1</sup>
As <sup>5+</sup>	0.03	3.6E-7	0.04	5.7E-7				
Ba <sup>2+</sup>	0.85	6.2E-6	1.36	9.9E-6	0.42	3.0E-3	0.67	4.9E-6
B <sup>3+</sup>	0.04	3.5E-6	0.06	5.6E-6				
Ca <sup>2+</sup>	10 401.63	2.6E-1	16 565.57	4.1E-1	11 987.61	3.0E+2	19 091.38	4.8E-1
Cr <sup>3+</sup>	0.02	4.5E-7	0.04	7.2E-7	0.29	5.6E-3	0.47	9.0E-6
Cu <sup>2+</sup>	0.06	9.3E-7	0.09	1.5E-6				
Li <sup>+</sup>	0.12	1.7E-5	0.13	1.9E-5	0.33	4.8E-2	0.35	5.1E-5
Mg <sup>2+</sup>	2 122.20	8.7E-2	3 379.80	1.4E-1	1 791.00	7.4E+1	2 852.33	1.2E-1

....Etc.

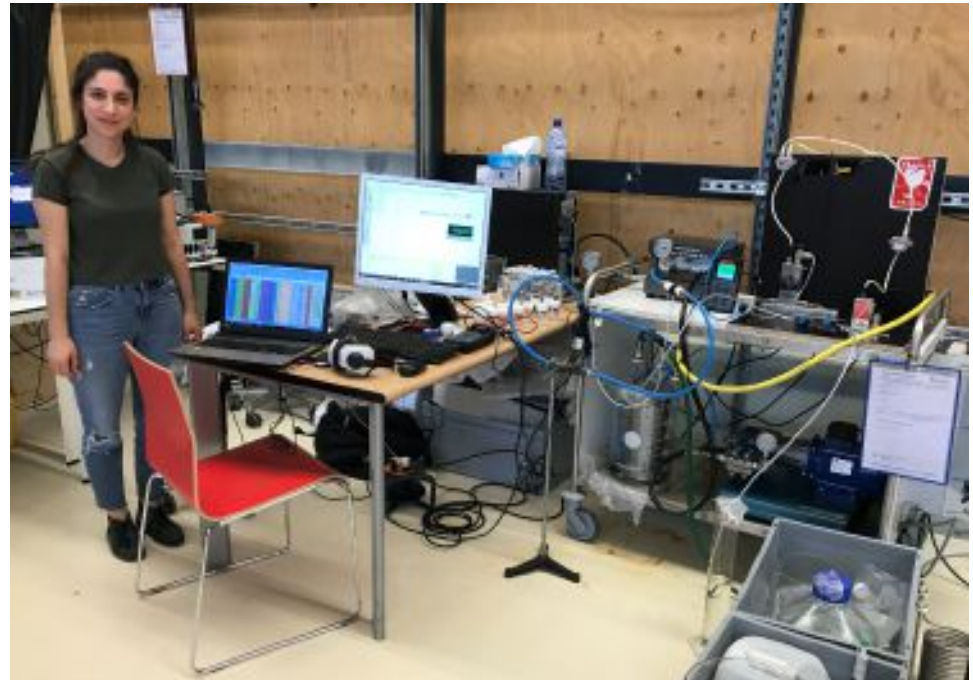
Mg and Ca may be separated with great efficiency from spent IEX regenerant, however complete (> 99%) recovery not possible. Esp. part of the Mg will end up as scaling before reaching the crystallization step.

## D2.2 Water analysis IEX regenerant

Cations		MW	Concentration	Anions		MW	Concentration
		g/mol	mM			g/mol	mM
Sodium	Na <sup>+</sup>	23.0	222.36 ± 201.63	Chloride	Cl <sup>-</sup>	35.5	691.94
Magnesium	Mg <sup>2+</sup>	24.3	44.81 ± 9.22	Fluoride	F <sup>-</sup>	19.0	0.00
Potassium	K <sup>+</sup>	39.1	4.95 ± 1.54	Bromide	Br <sup>-</sup>	79.9	0.00
Calcium	Ca <sup>2+</sup>	40.1	163.31 ± 0.79	Iodide	I <sup>-</sup>	126.9	17.52
Iron	Fe <sup>3+</sup>	55.8	0.02 ± 0.02	Nitrite	NO <sub>2</sub> <sup>-</sup>	46.0	0.00
Titanium	Ti <sup>2+</sup>	47.9	0	Nitrate	NO <sub>3</sub> <sup>-</sup>	62.0	0.00
Vanadium	V <sup>5+</sup>	50.9	3.18E-6 ± 2.16E-6	Phosphate	PO <sub>4</sub> <sup>3-</sup>	95.0	4.11
Chromium	Cr <sup>3+</sup>	52.0	9.61E-7 ± 9.85E-7	Sulphate	SO <sub>4</sub> <sup>2-</sup>	96.1	0.00
Lithium	Li <sup>+</sup>	6.9	1.78E-5 ± 9.36E-7	Silicate	SiO <sub>4</sub> <sup>4-</sup>	92.1	31.14
Beryllium	Be <sup>2+</sup>	9.0	0	Bicarbonate	HCO <sub>3</sub> <sup>-</sup>	61.0	
Aluminum	Al <sup>3+</sup>	27.0	0				
Manganese	Mn <sup>2+</sup>	54.9	8.42E-8 ± 1.19E-7				
Cobalt	Co <sup>2+</sup>	58.9	2.51E-7 ± 3.54E-7				
Nickel	Ni <sup>2+</sup>	58.7	1.40E-5 ± 1.48E-5				
Copper	Cu <sup>2+</sup>	63.5	2.69E-7 ± 3.80E-7				
Zinc	Zn <sup>2+</sup>	65.4	7.91E-7 ± 1.12E-6				
Strontium	Sr <sup>2+</sup>	87.6	3.53E-4 ± 8.77E-5				
Molybdenum	Mo <sup>4+</sup>	95.9	8.36E-8 ± 9.95E-8				
Silver	Ag <sup>+</sup>	107.9	1.16E-8 ± 1.59E-8				
Cadmium	Cd <sup>2+</sup>	112.4	1.56E-9 ± 2.21E-9				
Antimony	Sb <sup>5+</sup>	121.8	5.30E-8 ± 6.80E-8				
Barium	Ba <sup>2+</sup>	137.3	2.85E-5 ± 3.77E-6				
Thallium	Tl <sup>3+</sup>	208.4	1.25E-9 ± 1.77E-9				
Lead	Pb <sup>2+</sup>	207.2	1.43E-7 ± 2.02E-7				
Total Dissolved Solids (TDS)			40 456.42	mg/L			

## D2.3 Bench scale tests

- Ultra Filtration (Lenntech)
- Membrane Crystallization (UNIPA)
- Evaporation (NTUA)





# D2.7 Database: providers, managers and data recipients

Data providers



TU Delft  
LENNTECH  
UNIPA  
NTUA  
ARIVA  
Evides

Data acquisition



Database



TU Delft

Data distribution



Data recipients



Internal recipients

TU Delft  
LENNTECH  
UNIPA  
NTUA  
ARIVA  
Evides

External recipients

Public recipients  
WP1: TU Delft  
WP10: REVOLVE MEDIA  
WP7: IVL  
WP8: SEALEAU  
WP9: NTUA



Cooling Tower Huntsman

Central WWTP

Evides DWP

Plant One

Merseyweg 10

Chemical Plant  
Ducor Petrochemicals BV

Lucite International  
Holland BV

Bertschi B.V.

Chemical Plant  
Glimax Molybdenum

Arbo Unie Europort

Lyondell Chemie  
Nederland BV

EQIN

Google

Stork Safety &



# Plant One, Botlek



- Brine by IBC bulk containers
- Waste heat: condensate